Amendments to the Specification:

Please add the following heading at page 1, before line 2:

FIELD OF THE INVENTION

Please add the following heading at page 1, before line 7:

BACKGROUND OF THE INVENTION

Please delete the paragraph at page 1, line 23 through line 26.

Please add the following heading at page 4, before line 9:

SUMMARY OF THE INVENTION

Please add the following headings and paragraphs at page 5, after line 9:

BRIEF DESCRIPTION OF THE DRAWINGS

The invention is illustrated by reference to the accompanying drawing in which Fig. 1 is a diagrammatic flowsheet of an embodiment of the invention.

DETAILED DESCRIPTION OF THE INVENTION

In the present invention at least part of the tail gas is used for combustion in a gas turbine to provide power for the process. This leads to benefits in process power efficiency and may result in significant plant cost savings because the need for high-pressure steam turbine plant may be significantly reduced or eliminated.

Please replace the paragraph beginning at page 5, line 10, with the following rewritten paragraph:

Generally referring to the present invention, ~~T~~the amount of oxygen required in the secondary reformer is determined by two main considerations, viz. the desired composition of the product gas, and the heat balance of the heat exchange reformer. Thus generally

increasing the amount of oxygen causes the $[H_2]/[CO]$ ratio to decrease and the proportion of carbon dioxide to decrease. Alternatively, if the conditions are arranged such that the product composition and temperature is kept constant, increasing the temperature at which the feedstock is fed to the heat exchange reformer decreases the amount of oxygen (at a constant oxygen feed temperature) required. Decreasing the required amount of oxygen is advantageous as this means that a smaller, and hence cheaper, air separation plant can be employed to produce the oxygen. The temperature of the feedstock can be increased by any suitable heat source, which may, if necessary, be a fired heater, which of course can use air, rather than oxygen, for the combustion.

Please replace the paragraph beginning at page 5, line 29, with the following rewritten paragraph:

The hydrocarbon synthesis reaction is preferably a Fischer-Tropsch (F-T) reaction such as is well know in the~~ prior~~ art. In a F-T process a synthesis gas containing carbon monoxide and hydrogen is reacted in the presence of a catalyst, which is typically a cobalt- and/or iron-containing composition. The F-T reactor type may be fixed bed, slurry reactor type or other suitable reactor configuration know to those skilled in the art. The desired products are liquid hydrocarbons (F-T hydrocarbons) which are separated, usually in a first separation stage with formed water, from the gaseous reaction products that contain unreacted gasses. Part of the gaseous reaction products stream is usually recycled to the F-T process, however in order to avoid a build-up of inert gasses in the process, a purge stream of F-T tail gas is also separated from the reaction products stream.

Please delete the paragraph beginning at page 7, line 16 through line 17.

Please replace the paragraph beginning at page 7, line 18, with the following rewritten paragraph:

In~~ the drawing~~ Fig. 1, a mixture of a desulphurised hydrocarbon feedstock, for example natural gas, and steam is fed, typically at a pressure in the range of 10 to 50 bar abs., via line 10 to a heat exchanger 12 and thence, via line 14, to the catalyst-containing tubes 16 of a heat exchange reformer 18. The mixture is typically heated to a temperature in the range 350 to

550°C prior to entry into the tubes 16. For simplicity only three tubes are shown in the drawing: in practice there may be several tens or hundreds of such tubes.